

Table 1. An example of sensitivity analysis

j	Parameter (p_j)			$\frac{\partial F}{\partial p_j}$	$\Delta p_j^{(*)}$	ΔF_j
	Symbol	Nominal Value	Units			
1	c_f	2.0×10^{-5}	\$/kJ	7.7378×10^{-2}	2.0×10^{-7}	1.5476×10^{-2}
2	c_e	8.33×10^{-6}	\$/kJ	2.3541×10^{-2}	8.33×10^{-7}	1.9610×10^{-2}
3	b_{11}	740.	$\$/(\text{kW})^{0.8}$	3.7912×10^{-3}	74.	2.8055×10^{-3}
4	b_{12}	0.8	-	2.8941×10^{-1}	0.08	2.3153×10^{-2}
5	b_{21}	3000.	$\$/(\text{kW})^{0.7}$	7.2855×10^{-6}	300.	2.1857×10^{-3}
6	b_{22}	0.7	-	2.1645×10^{-1}	0.07	1.5152×10^{-2}
7	b_{31}	217.	\$/m ²	1.2885×10^{-5}	21.7	2.7961×10^{-3}
8	b_{32}	577.	\$/ (kg/s)	5.7447×10^{-6}	57.7	3.3147×10^{-3}
9	b_{41}	378.	$\$/(\text{kW})^{0.71}$	6.4086×10^{-7}	37.8	2.4225×10^{-3}
10	b_{42}	0.71	-	1.1835×10^{-3}	0.071	8.4029×10^{-3}
11	f_m	1.06	-	5.3079×10^{-2}	0.106	5.6264×10^{-3}
12	C	18.2	%	3.0914×10^{-3}	1.82	5.6264×10^{-3}
$\Delta F_{\max} = 7.0940 \times 10^{-2}$				$\Delta F_{\text{prob}} = 1.0813 \times 10^{-3}$		
(*) for $\Delta p_j/p_j = 0.10$						

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APPENDIX A

Expressions for the Functions of Fig. 2 and 3

The essergy flows related to the environment are:

$$y_{1,1} = \dot{e}_f, \quad y_{3,2} = \dot{M}_w v_w (P_2 - P_0) / \eta_{Mw}, \\ y_{4,1} = \dot{W}_4 = \dot{M}(h_4 - h_3) / \eta_{M4}, \quad y_{2,1} = \dot{W} = \eta_{M2} \dot{M}(h_1 - h_2).$$

Other essergy flows are:

$$y_{1,2} = \dot{M} v_4 (P_4 - P_1), \quad y_{2,1} = \dot{M}(\psi_1 - \psi_2), \quad y_{3,1} = \dot{M}(\psi_2 - \psi_3), \\ y_{4,1} = \dot{M}(\psi_4 - \psi_3), \quad \Psi_1 = \Psi_3 + y_{4,1} - y_{1,2} = \dot{M}[\psi_4 - v_4(P_4 - P_1)], \\ y_{1,1} = \Psi_1 - \Psi_1 = \dot{M}[\psi_1 - \psi_4] + v_4(P_4 - P_1),$$

where ψ is the flow essergy per unit mass:

$$\psi = h - h_0 - T_0(s - s_0) \quad \text{and} \quad \Psi = \dot{M}\psi.$$

The negentropy flows are:

$$y_{3,1} = \dot{S}_2 - \dot{S}_3 \rightarrow y_{3,1} = \dot{M}T_0(s_2 - s_3), \\ y_{1,3} = \dot{S}_1 - \dot{S}_4 \rightarrow y_{1,3} = \dot{M}T_0(s_1 - s_4), \\ y_{2,2} = \dot{S}_2 - \dot{S}_1 \rightarrow y_{2,2} = \dot{M}T_0(s_2 - s_1), \\ y_{4,2} = \dot{S}_4 - \dot{S}_3 \rightarrow y_{4,2} = \dot{M}T_0(s_4 - s_3),$$

where:

$$\dot{S}_i = -\dot{M}s_i \quad (i = 1, 2, 3, 4).$$

The last forms of $y_{3,1}$, $y_{1,3}$, $y_{2,2}$, and $y_{4,2}$ are obtained by multiplying negentropy flows by the reference temperature T_0 and changing the sign. This convenient procedure is used in order to obtain all functions as positive quantities in the same units.

APPENDIX B

Cost Functions

The following equations have been derived in Ref. 5 by using information from several sources (e.g. Refs. 11-14):

$$Z_1 = \zeta_{11} y_{1,1}^{\beta_1} \zeta_{p1} g_{11} g_{1T}, \quad Z_2 = \zeta_{21} y_{2,1}^{\beta_2} \zeta_{p2} g_{2T}, \\ Z_3 = T_2 (\zeta_{31} n_3 R_3 + \zeta_{32} / c_{pw}) y_{3,1} / [T_0 (T_0 - T_2)], \\ Z_4 = \zeta_{41} y_{4,1}^{\beta_4} \zeta_{p4} g_{4T}, \quad \Gamma_{0,k} = c_k y_{0,k} \quad (k = 1, 2, 3),$$

where:

$$\zeta_{ri} = (C/3.6 \times 10^3 N) \phi_i b_{ri}, \quad g_p = \exp[(P_i - \bar{P}_1)/b_{13}], \\ g_{1T} = 1 + [(0.45 - \eta_{11})/(0.45 - \eta_0)]^{\beta_{1T}}, \\ g_{rT} = 1 + b_{rs} \exp[(T_1 - \bar{T}_1)/b_{r6}] \quad (r = 1, 2), \\ g_{r\eta} = 1 + [(1 - \eta_{1r})/(1 - \eta_{10})]^{\beta_{r\eta}} \quad (r = 2, 4).$$

Z_1 - Boiler

Z_2 - ST

Z_3 - condenser

Z_4 - pump